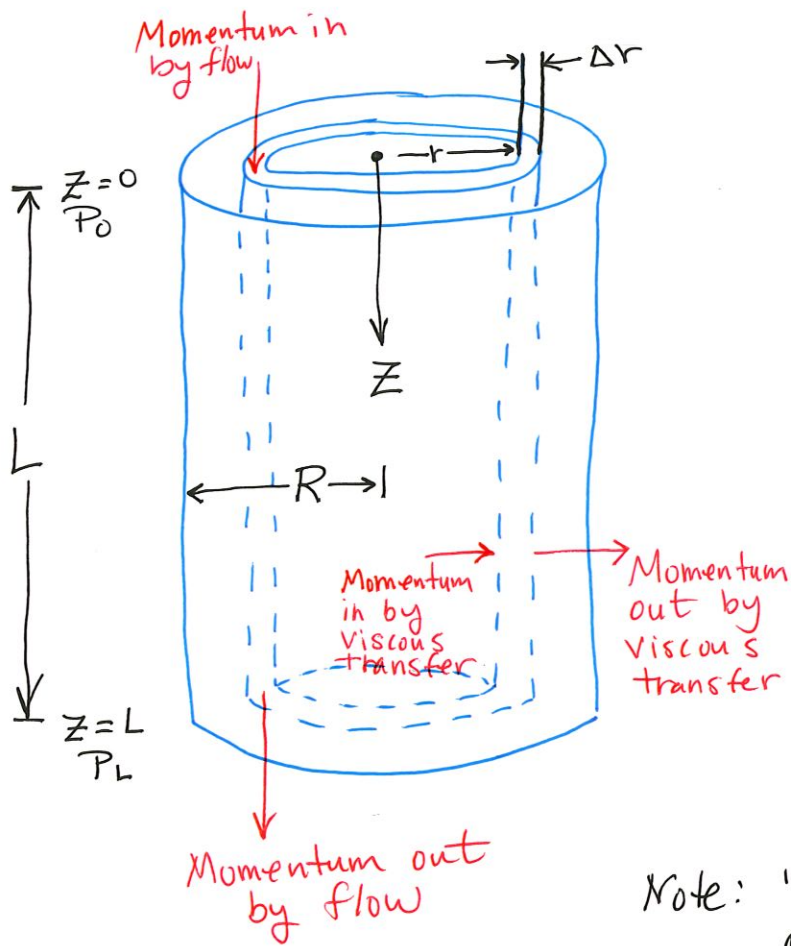


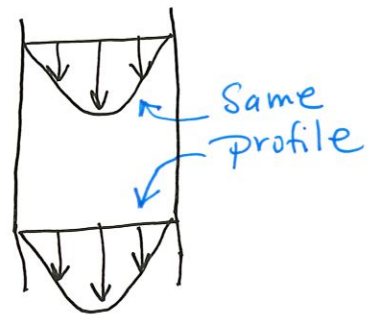
Lecture 3 : Momentum Balance

Consider flow of a fluid in a pipe



Assume:

1. $\rho = \text{constant}$
2. Laminar flow
3. Fully developed flow (no z dependence)



4. Steady state
5. No slip at wall

Note: "in" and "out" arrows are taken in the positive r & z directions

$$\text{Production of momentum} = \sum F$$

$$\text{Inflow} - \text{Outflow} + \sum F = 0 \quad (\text{accumulation} = 0)$$

Momentum balance (momentum/time): ?

Divide by $2\pi L \Delta r$, take limit $\Delta r \rightarrow 0$

$$\frac{d}{dr} r \tau_{rz} = \left(\frac{P_0 - P_L}{L} + \rho g \right) r = \left(\frac{P_0 - P_L}{L} \right) r$$

Integrate: $\tau_{rz} = \frac{P_0 - P_L}{2L} r + \frac{C_1}{r}$

$P = P_0 - \rho g z$

$C_1 = 0$ so term does not go to ∞

Assume Newton's Law: $\tau_{rz} = -\mu \frac{dv_z}{dr}$

$$\frac{dv_z}{dr} = - \left(\frac{P_0 - P_L}{2\mu L} \right) r$$

Integrate to yield:

$$v_z = - \frac{(P_0 - P_L)}{4\mu L} r^2 + C_2$$

But $v_z = 0$ at $r = R$ so that

$$v_z = \frac{(P_0 - P_L)}{4\mu L} R^2 \left(1 - \left(\frac{r}{R} \right)^2 \right)$$

"Hagen Poiseuille" law

Parabolic velocity profile

Other results

$$v_{z, \max} = \left(\frac{P_0 - P_L}{4\mu L} \right) R^2 = 2 \langle v_z \rangle$$

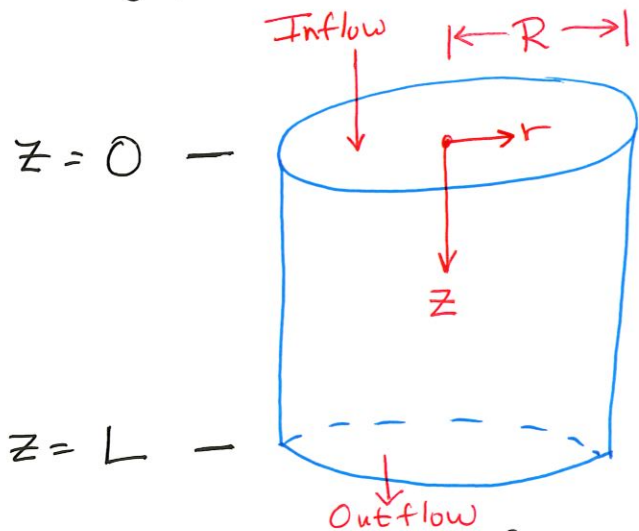
Average velocity \downarrow

$$\langle v_z \rangle \pi R^2 = Q = \frac{\pi (P_0 - P_L)}{8\mu L} R^4$$

volume flow \uparrow

By definition: $\langle v_z \rangle = \int_0^R 2\pi r v_z dr / \pi R^2$

Macroscopic momentum balance on fluid in pipe
 (inflow - outflow + $\sum F = 0$)



Result: Net pressure force + shear force + gravitational force = 0

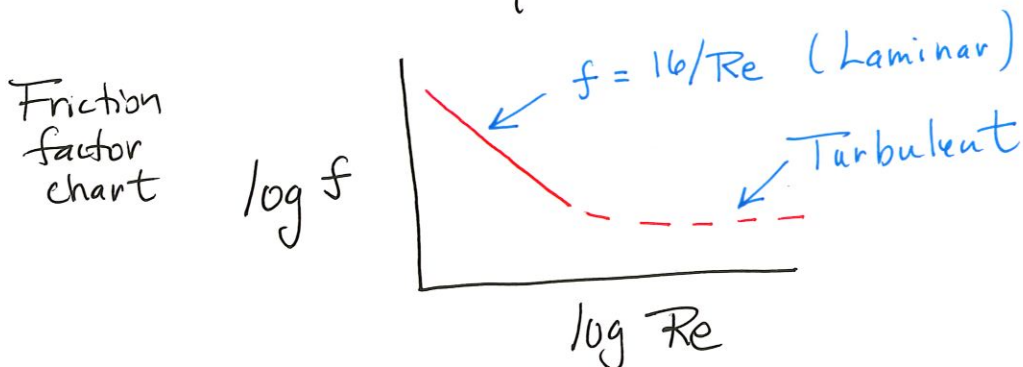
Define friction factor f

$$f = \frac{\tau_{rz}|_{r=R}}{\frac{1}{2} \rho \langle v_z \rangle^2} = \frac{(\mathcal{P}_0 - \mathcal{P}_L) R}{L \rho \langle v_z \rangle^2} = \frac{R \langle v_z \rangle 8 \mu L}{L \rho \langle v_z \rangle^2 R^2}$$

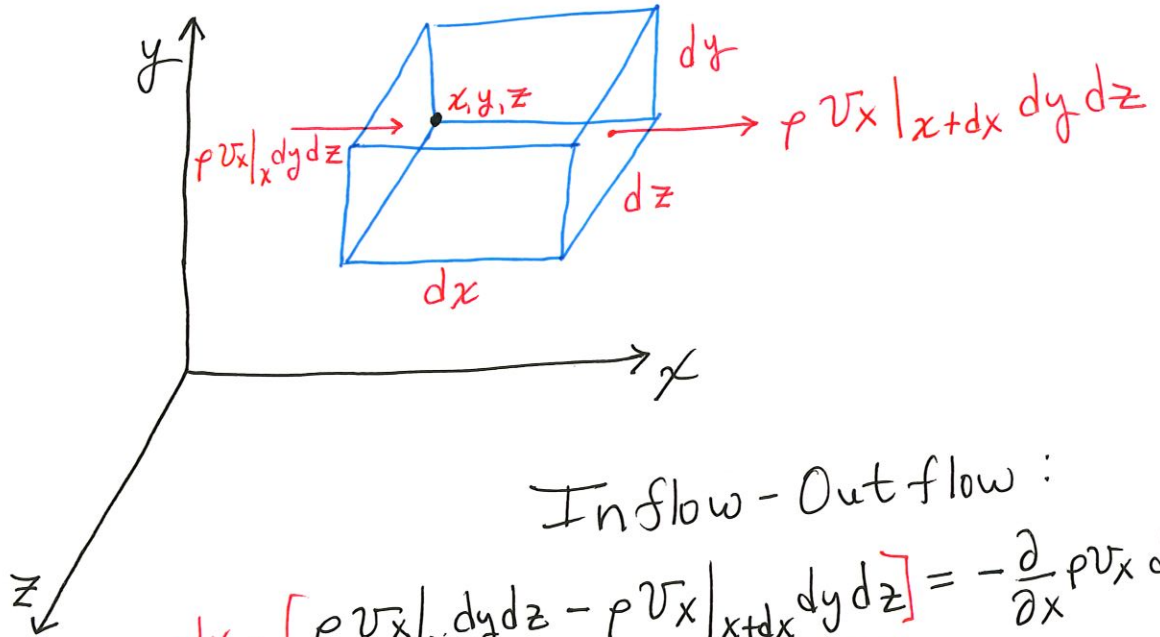
Substitute from previous page to eliminate $(\mathcal{P}_0 - \mathcal{P}_L)$

Kinetic energy per unit volume

$$f = \frac{16}{\rho \langle v_z \rangle D / \mu} = \frac{16}{Re}$$



More general approach (for Cartesian coordinates)
 Mass balance (in terms of mass/sec)



Inflow - Outflow:

$$dx \cdot \left[\rho v_x|_x dy dz - \rho v_x|_{x+dx} dy dz \right] = -\frac{\partial}{\partial x} \rho v_x dx dy dz$$

Mass balance:

$$\frac{\partial \rho}{\partial t} dx dy dz = - \underbrace{\frac{\partial}{\partial x} \rho v_x dx dy dz}_{x \text{ direction}} - \underbrace{\frac{\partial}{\partial y} \rho v_y dx dy dz}_{y \text{ direction}} - \underbrace{\frac{\partial}{\partial z} \rho v_z dx dy dz}_{z \text{ direction}}$$

Divide by $dx dy dz$:

$$\frac{\partial \rho}{\partial t} = - \left(\frac{\partial \rho v_x}{\partial x} + \frac{\partial \rho v_y}{\partial y} + \frac{\partial \rho v_z}{\partial z} \right)$$

$$= - \underbrace{\nabla \cdot \rho \vec{v}}_{\text{mass flux}}$$

mass efflux/unit volume

Special forms: steady state $\Rightarrow \nabla \cdot \rho \vec{v} = 0$

$\rho = \text{constant} \Rightarrow \nabla \cdot \vec{v} = 0$

Can also be written as: $D\rho/Dt = -\rho (\nabla \cdot \vec{v})$ -4-