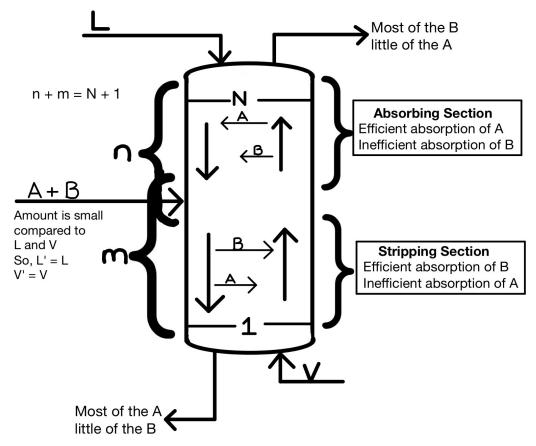
Special Topics Related to Staged Processes

Two section absorber/ stripper for the fraction of mixture A and B

For KB > KA:



Reduces to absorber form of KSB equation if m = 1, n = N and $y^*_{out} = 0$

Two section KSB equation:

SB equation:
$$\frac{V_{i,N}}{L_{i,1}} = \left(\frac{K_{i}V}{L}\right) \left[\frac{\left(\frac{K_{i}V}{L}\right)^{n} - 1}{\left(\frac{K_{i}V}{L}\right)^{n} - 1}\right]$$

Top section:

Efficient absorbing of A

$$\frac{L}{K_{AV}} > I \Rightarrow \frac{L}{V} > K_{A}$$

Inefficient absorbing of B

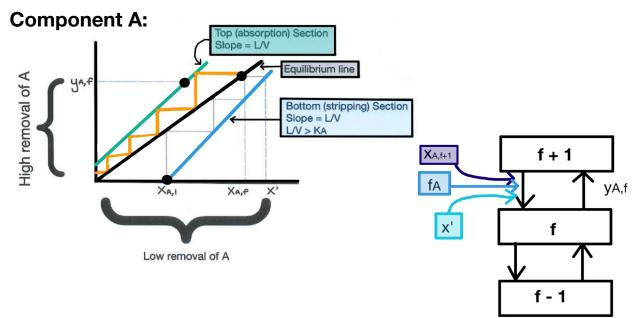
$$\frac{L}{K_BV}$$
 < 1 \Rightarrow $\frac{L}{V}$ < K_B

Bottom section:

Efficient stripping of B

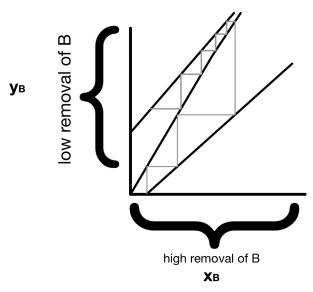
Inefficient stripping of A

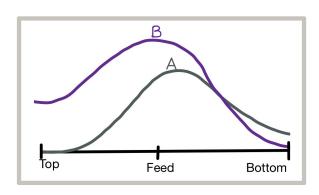
All 4 conditions are satisfied if: $K_B > \frac{L}{V} > K_A$ Often the optimal value for $\frac{L}{V}$ is given by: $\sqrt{K_AK_B}$



Material balance at feed point fA + (xA,f+1)(L) = x'L

Component B:



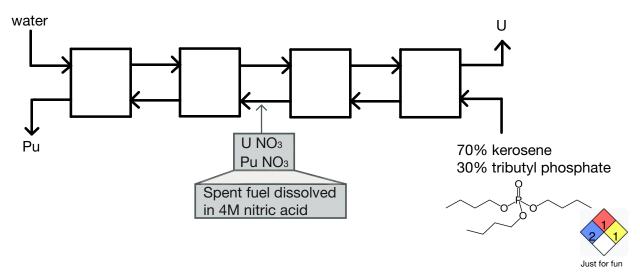


Staged extraction for fractionation of solutes

Examples:

PUREX Process-

Plutonium Uranium Extraction

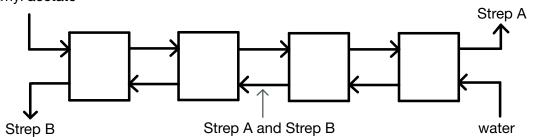


Production of Streptomycin (an antibiotic)

Final step is the removal of Streptomycin B from the active form (Strep. A)

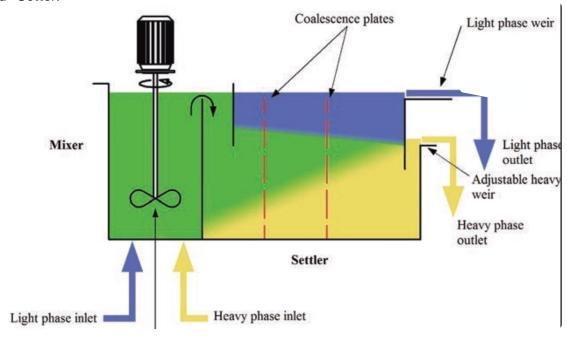
3

amyl acetate



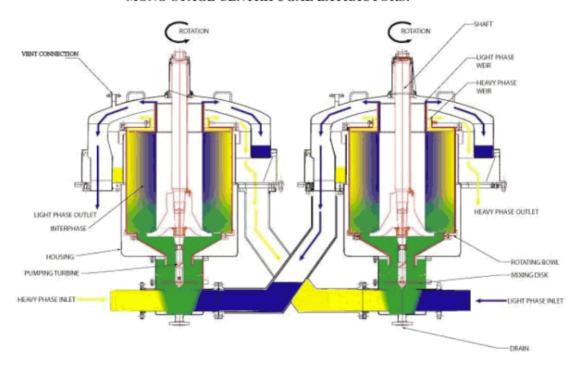
Extraction Equipment

Mixed- Setter:

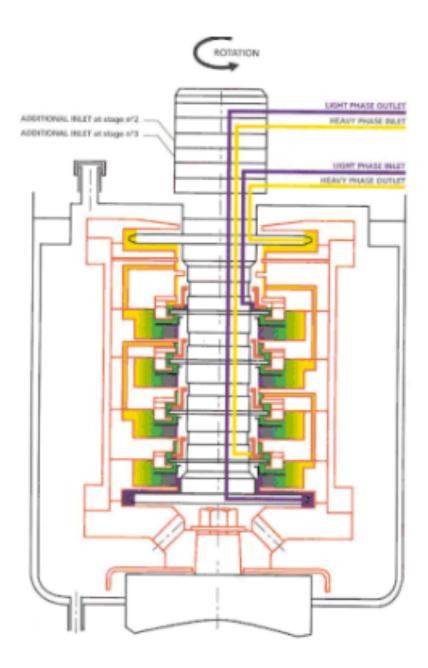


Centrifugal Extractor:

MONO-STAGE CENTRIFUGAL EXTRACTORS:

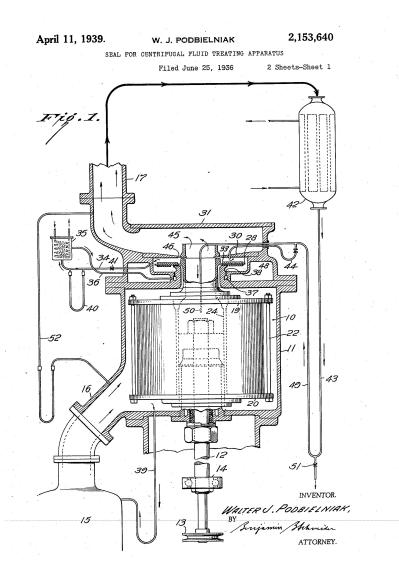


Cross section sketch of 4 stage centrifugal extractor

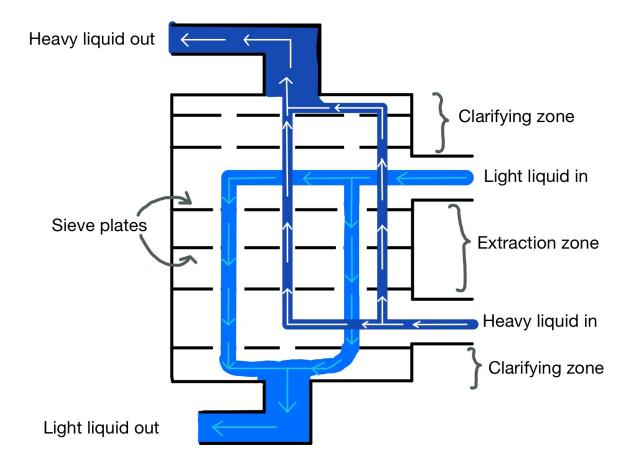


The Podbielniak extractor Invented by Walter J. Podbielnick

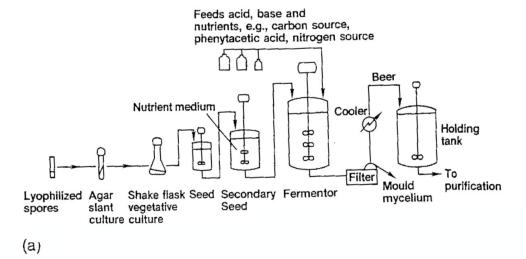




Operates like a sieve plate tower



Penicillin



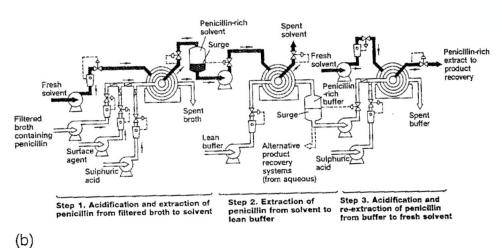


Figure 8.7. (a) Penicillin fermentation flow sheet, illustrating the inoculum stages. (b) The recovery train for penicillin.